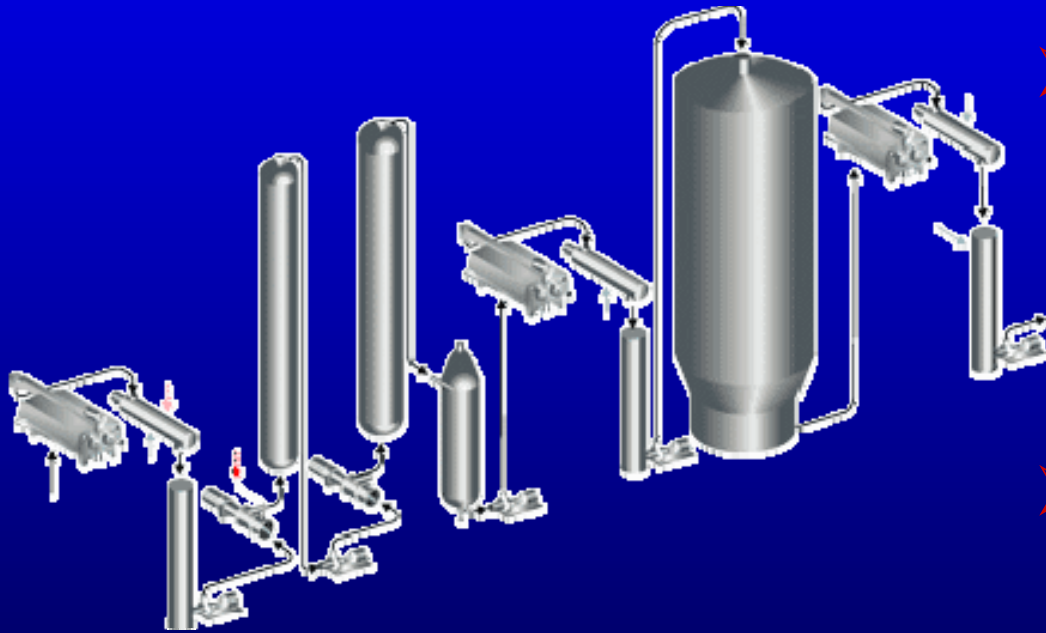


*Mini Oxygen Stages for SW Kraft Pulps  
More Delignification with Less Capital*

Art J. Ragauskas

# Evolution of Oxygen Delignification

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## ➤ 1960/70s

- Basic engineering
- General chemistry

## ➤ 1980/early 1990s

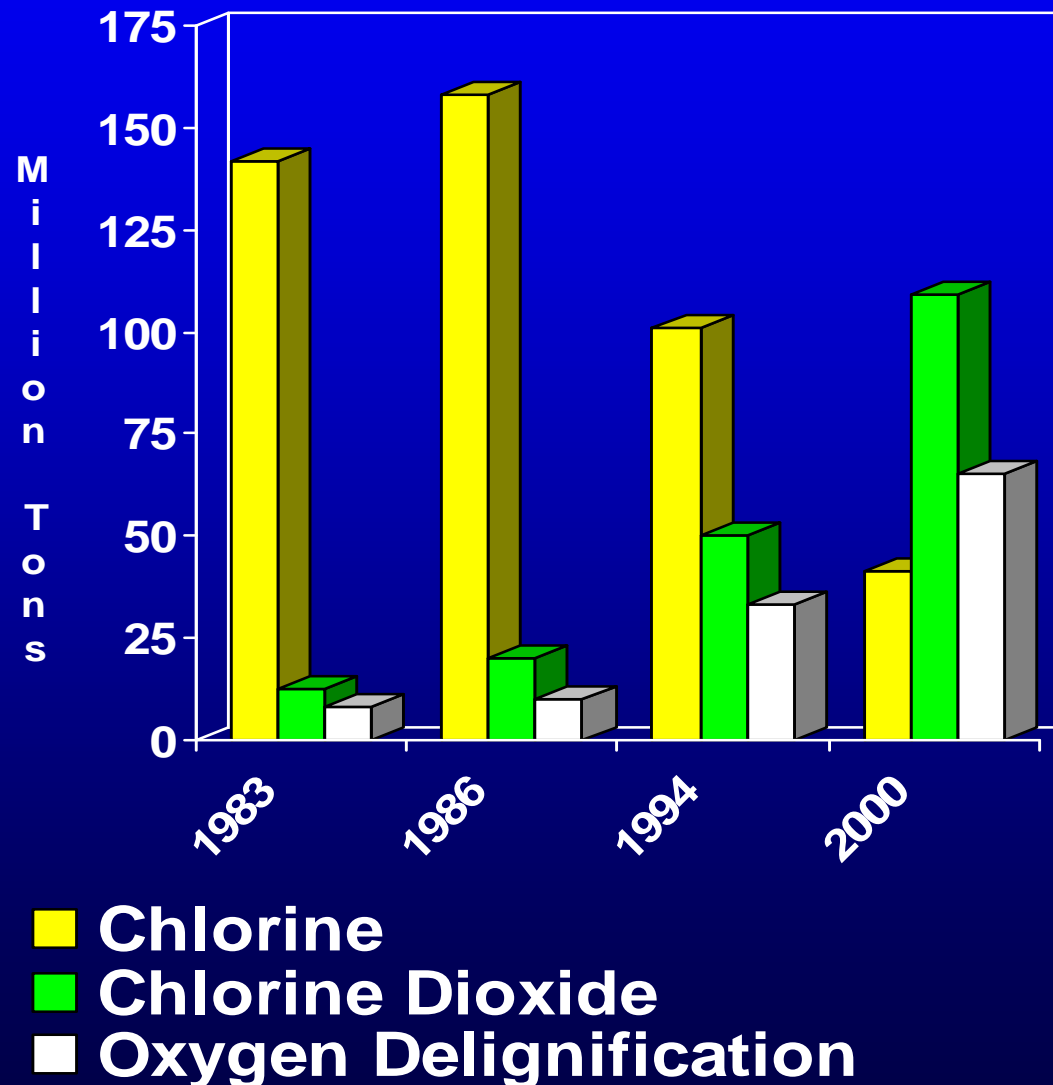
- Process variables, energy, environmental, pretreatments
- Fundamental chemistry & pulp properties

## ➤ Late 1990s/2000

- Yield, selectivity, process parameters,
- Lignin/carbohydrate chemistry, catalysis

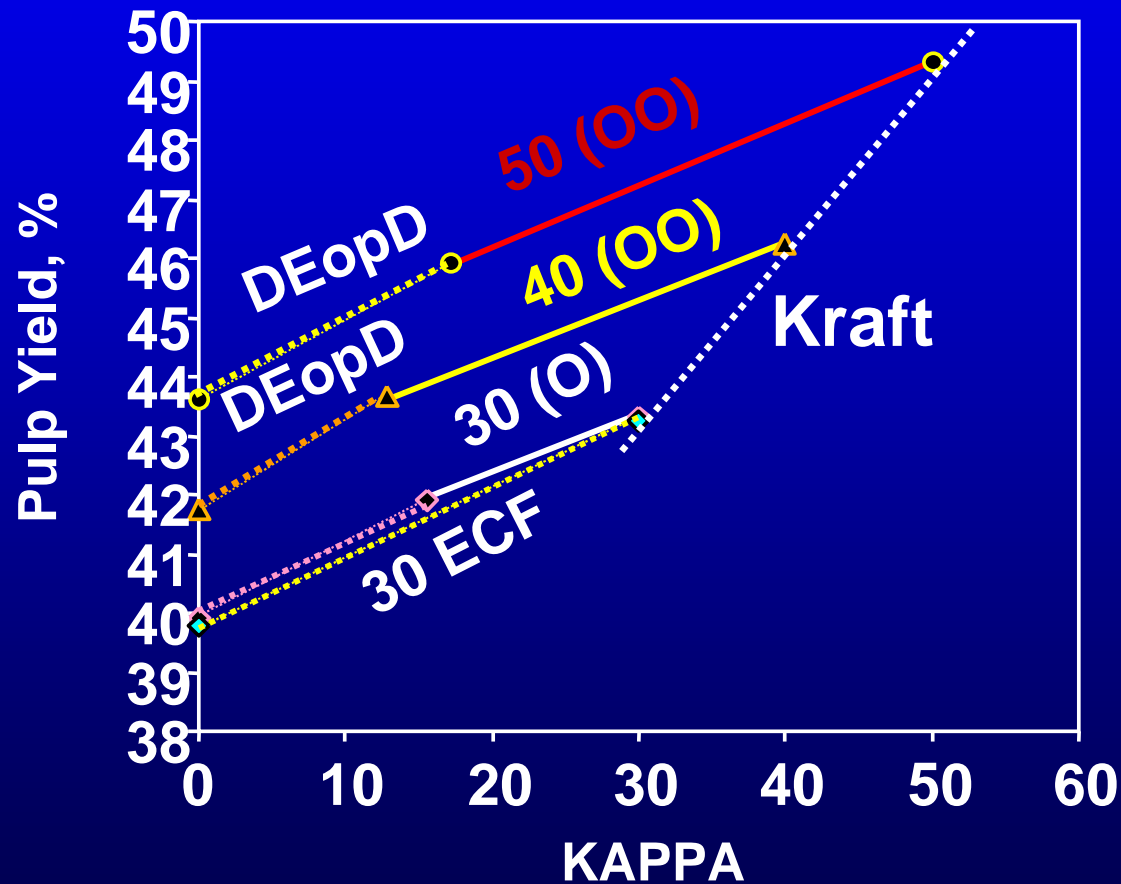
# Application in North American Bleach Plants

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# Increased Selectivity, Yield, and Environmental Performance

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Jameel, H. "High Kappa Pulping and Extended Oxygen Delignification to Increase Yield,"  
1998 TAPPI Proceedings: Breaking the Yield Barrier Symposium, pps. 165-182.

*ragauskas@hotmail.com*

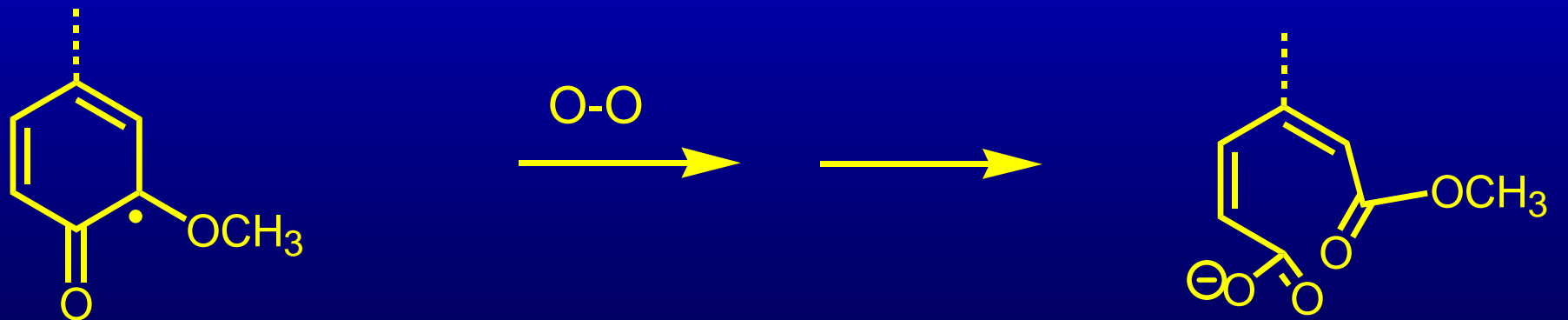
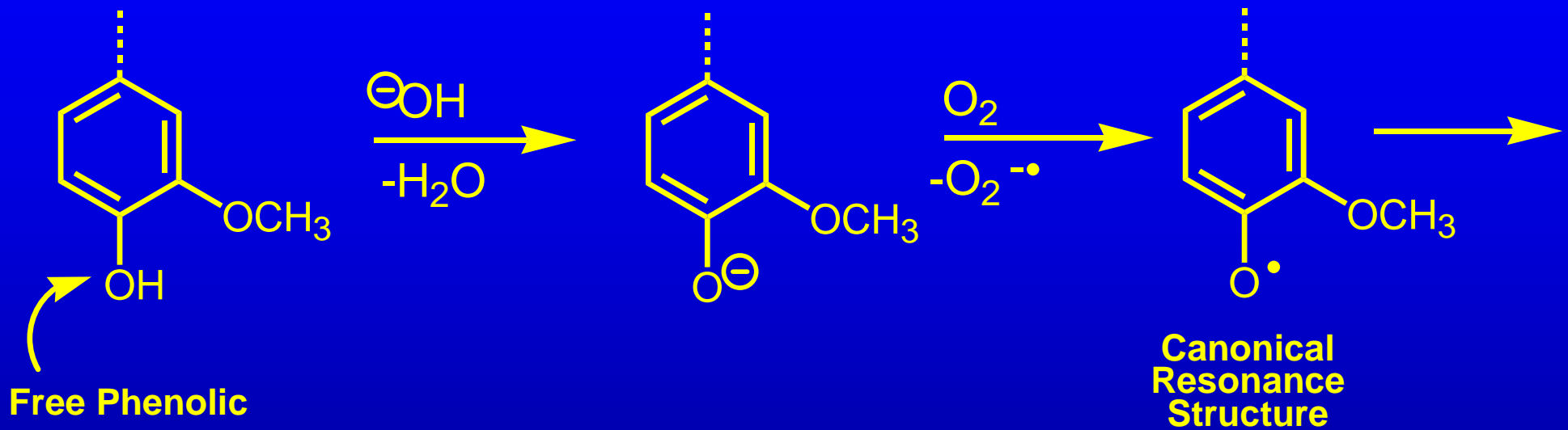
# *Chemistry of Oxygen Delignification*

# Oxidative Agents

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Species	Oxidative Result
Superoxide ( $O_2^{\cdot-}$ )	Addition to ring
Hydroperoxide ( $O_2H^{\cdot}$ )	Addition to ring, ketones, aldehydes
Hydroxyl ( $OH^{\cdot}$ )	Severe oxidation and fragmentation
Oxoanion ( $O^-$ )	Attack of rings and carbohydrates

# Oxidation of Lignin



**Muconic Methyl Ester**

# Research Attention

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## ➤ APPLIED

- Oxygen delignification addresses the top P&P research need for increased mill closure (*TAPPI Workshop Paper Industry Research Needs, 1996*)
- Mini oxygen systems have not been as thoroughly investigated as warranted by capital cost effectiveness and performance

## ➤ FUNDAMENTAL

- The number of citations has risen to over 100/year
- The chemical mechanisms are controversial



# Research Objective I

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**Examine the chemical similarities and differences in typical SW kraft pulp after standard O and mini O stages**

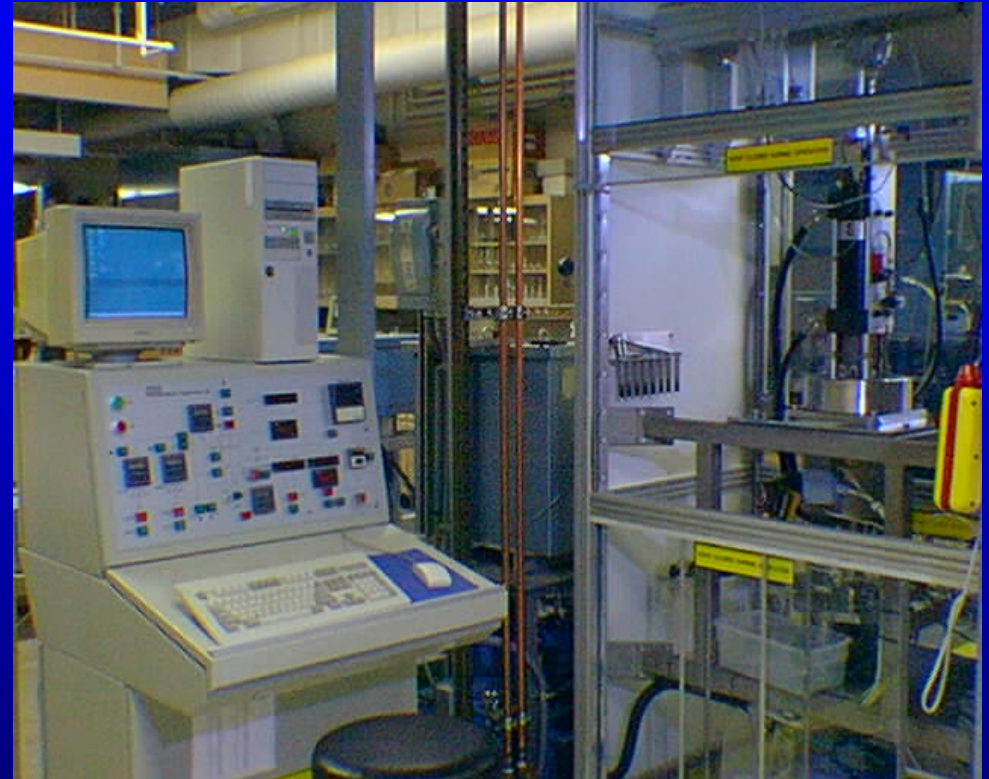
- **% Delignification**
- **Viscosity**
- **Fundamental lignin structures**

# Experimental Design

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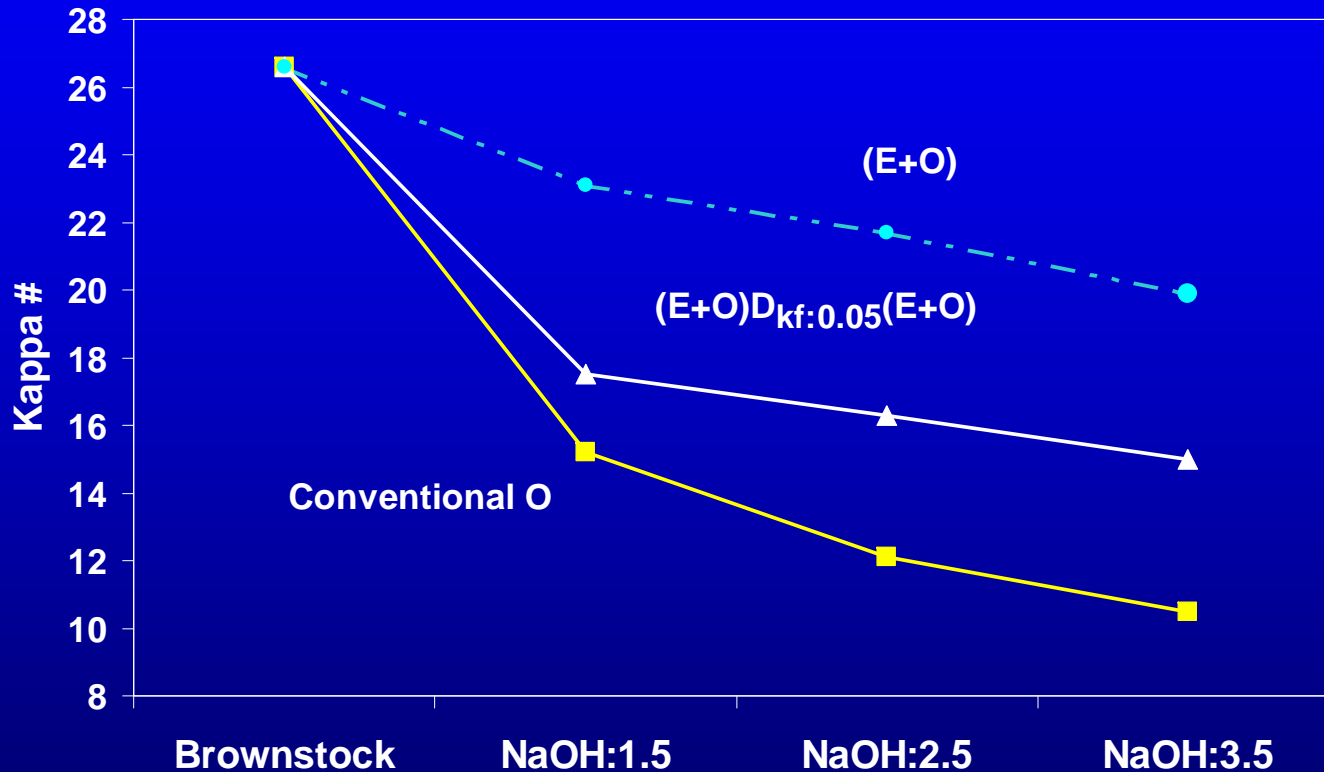
## Bleaching Conditions

- **O Stage: 10% cn., 90°C, 60 min., 2.5% NaOH odw**
- **D Stage: 2 kappa factors used – 0.05 and 0.20 ( $D_0$ ) at 10% cn., 70°C, 30 min.**
- **(E+O): 10% cn., 90°C, 20 min., 1.25% NaOH odw**
- **(E+O)\*: 10% cn., 90°C, 40 min., 2.5% NaOH odw**



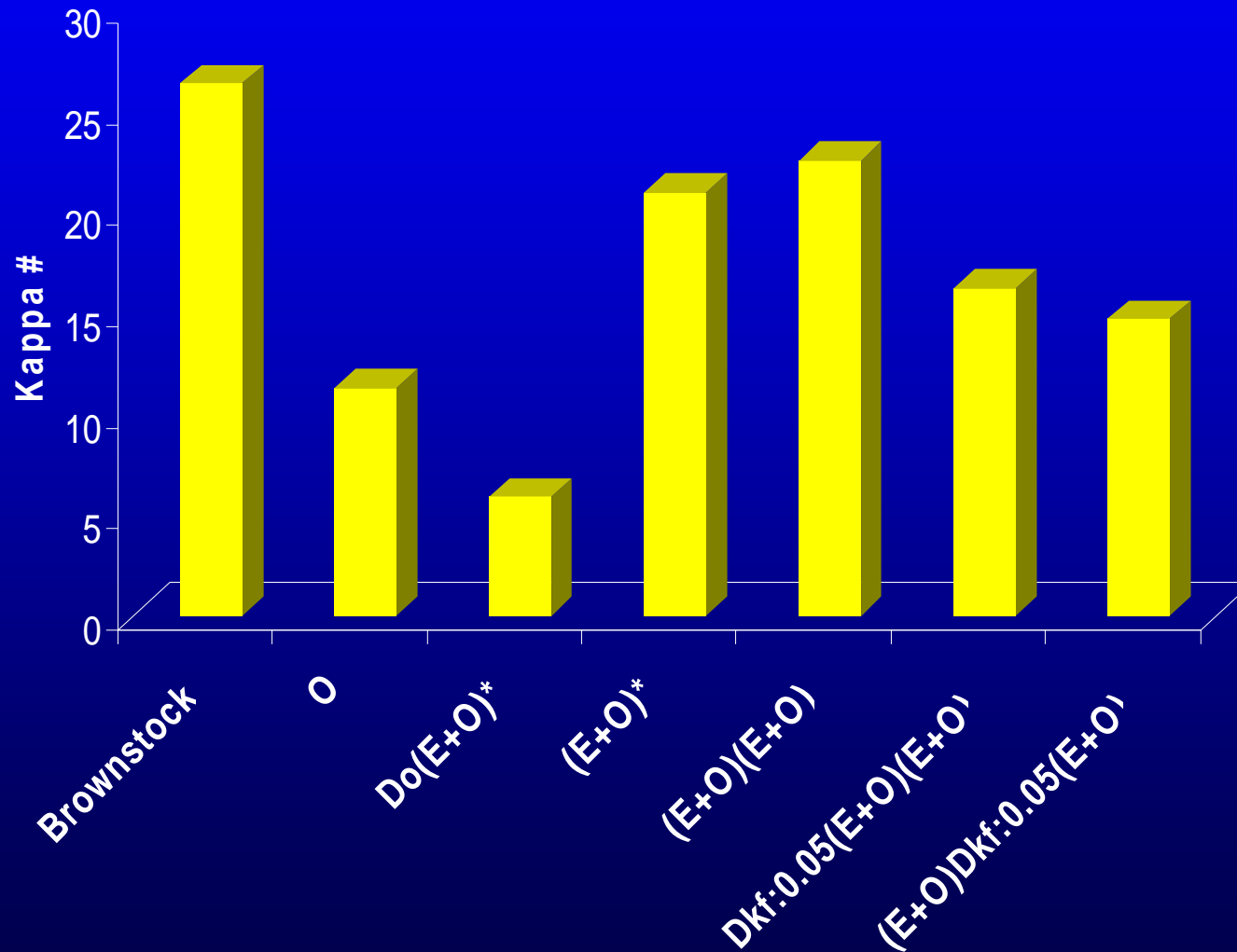
# *Oxygen Delignification Results*

# SW Kraft Pulp Delignification



- (E+O) provides up to 25% delignification
- At low caustic, the mini-O, (E+O)D(E+O), performs within 5% as well as a standard O
- By splitting caustic charge in mini-O, the interstage D stage enhanced performance of subsequent (E+O)

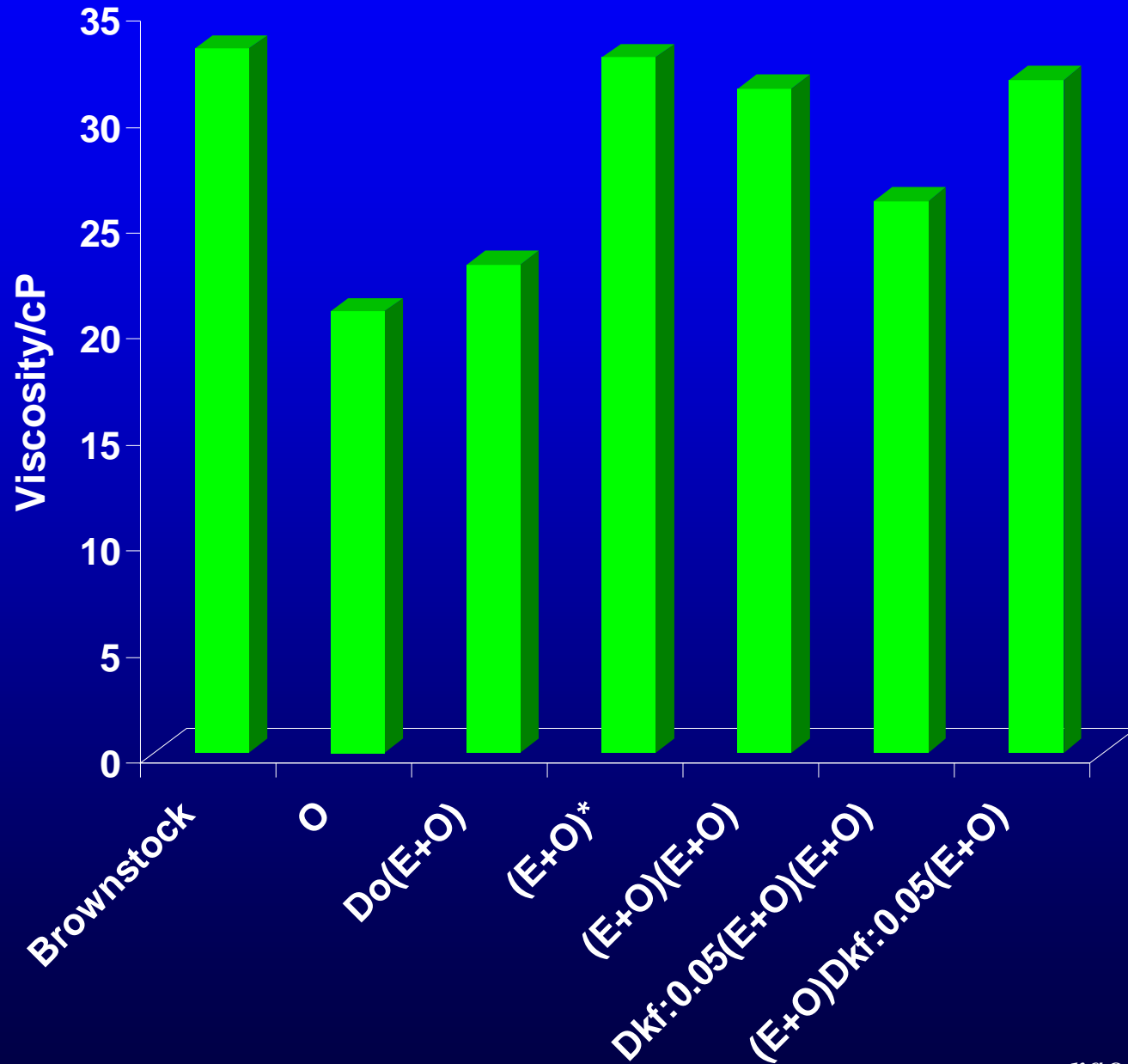
# Delignification from Mini O



- Splitting caustic charge is not as effective as one dose in (E+O)\*
- Placement of low kappa factor charge impacts the final delignification level
- (E+O) strongly complements the D<sub>0</sub>

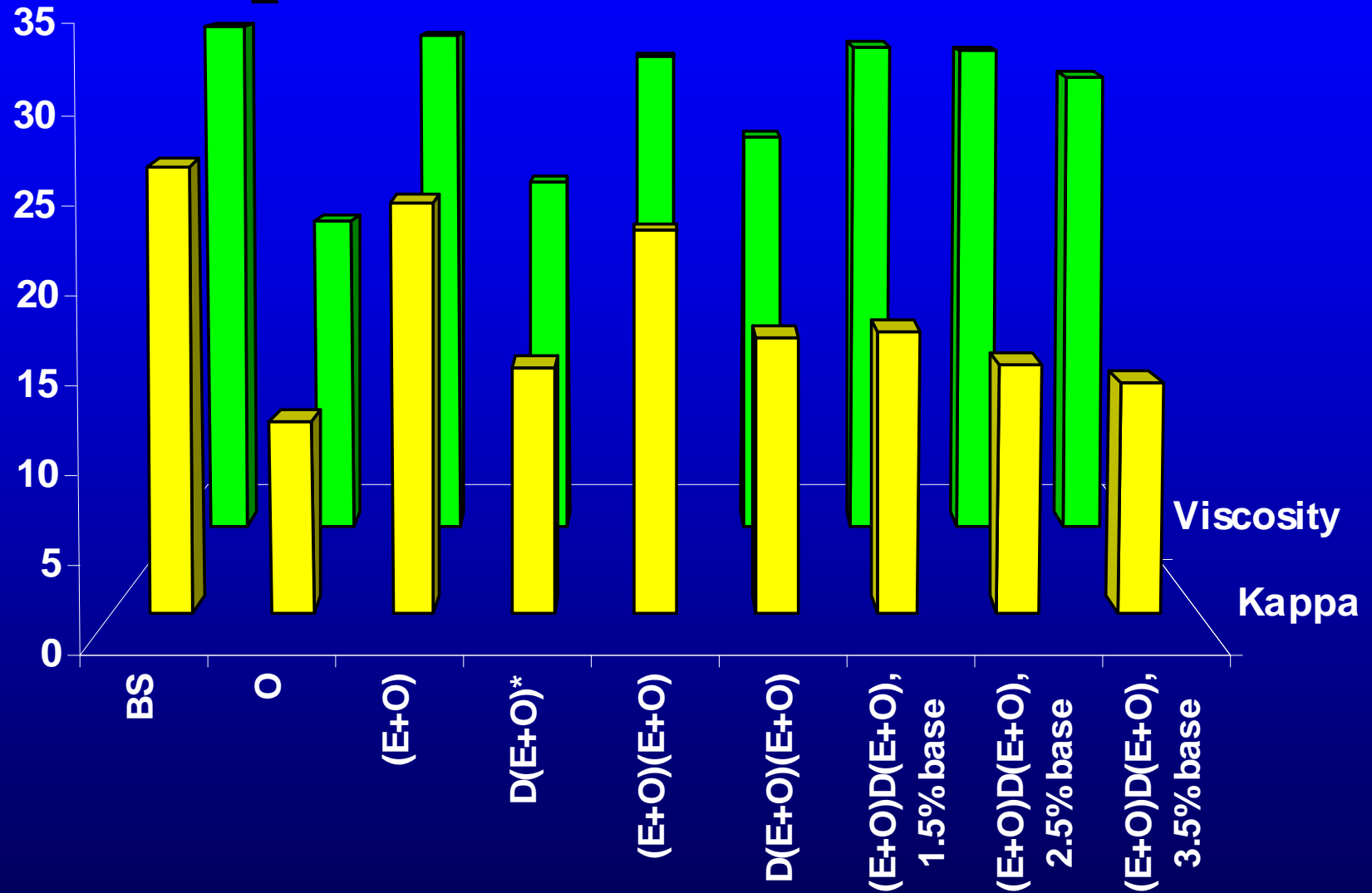
# Viscosity from Mini O Trials

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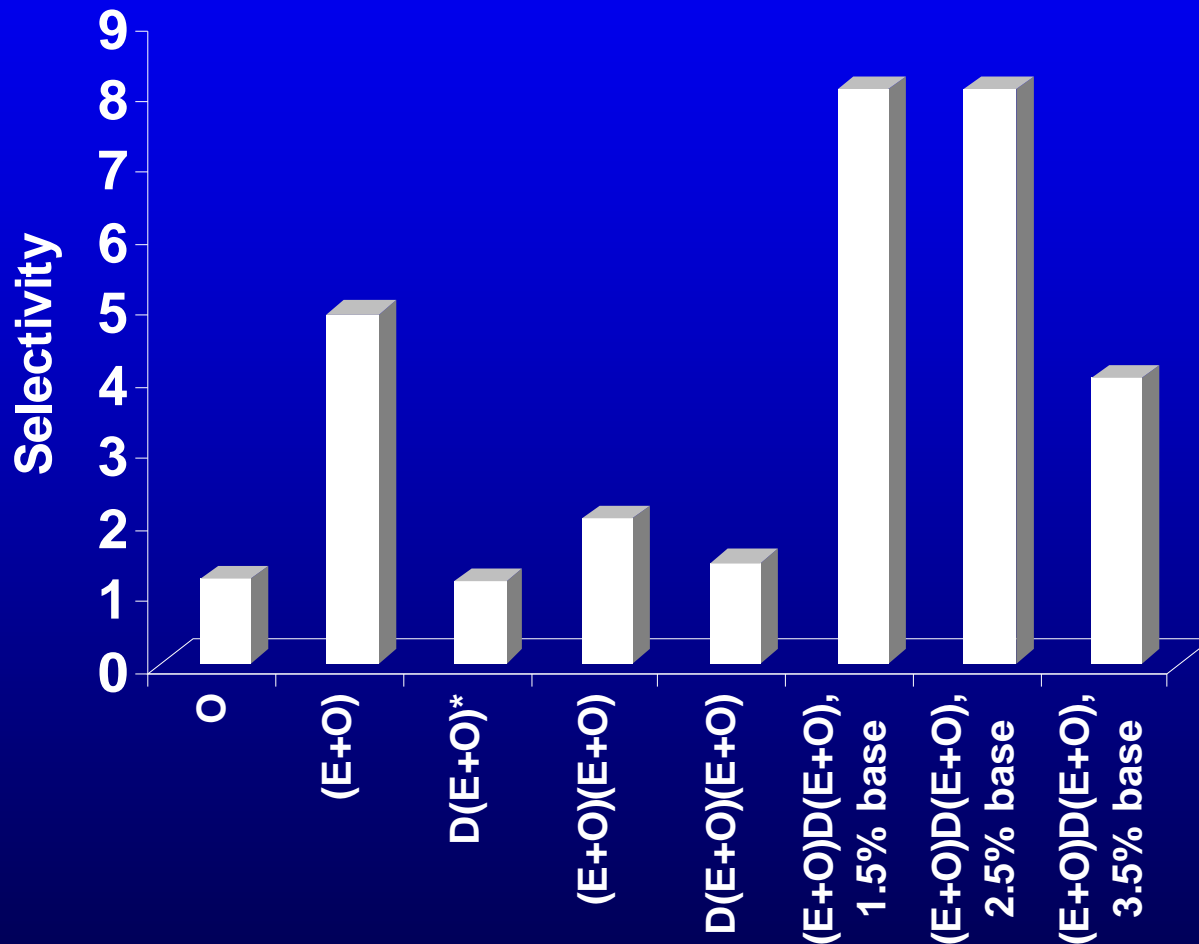
# Kappa Viscosity

## Comparison of Mini O Trials



A mini O stage is less sensitive to base induced pulp degradation than a full O

# Selectivity of Mini O

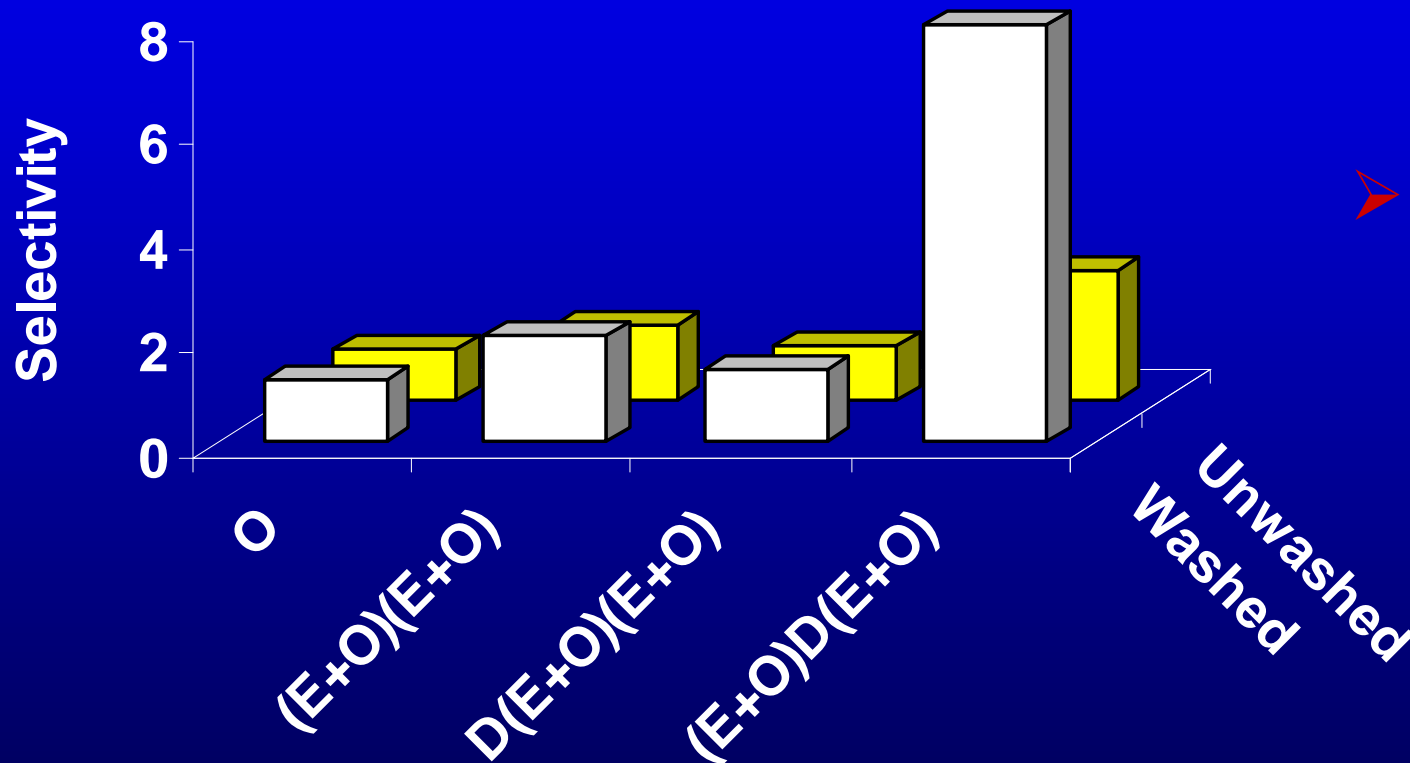


- (E+O) stage provides more selectivity than a full O
- The D stage placement is critical to the overall performance of the mini O



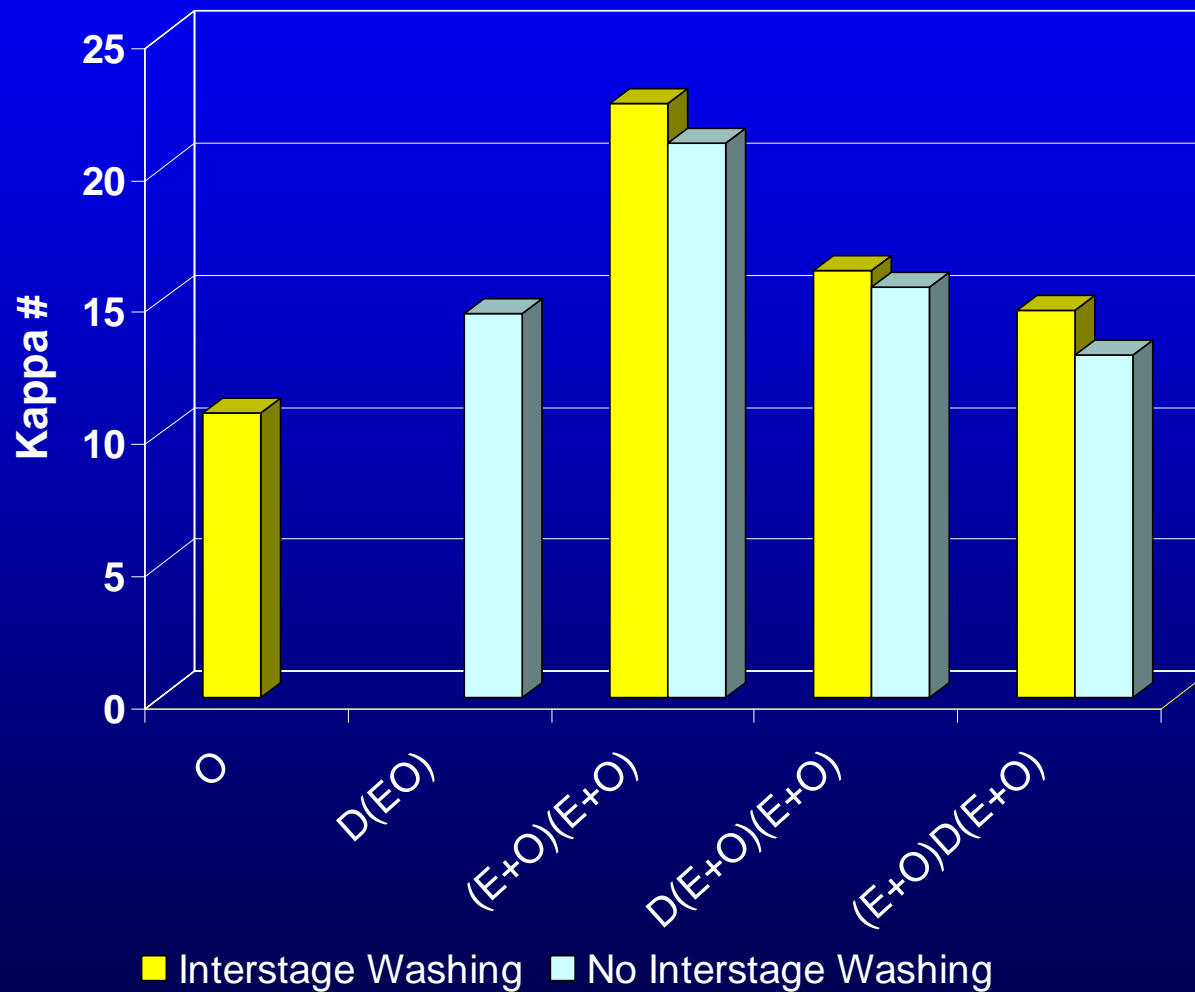
# *Influence of Washing and Carryover*

# Effect of Washing on Selectivity



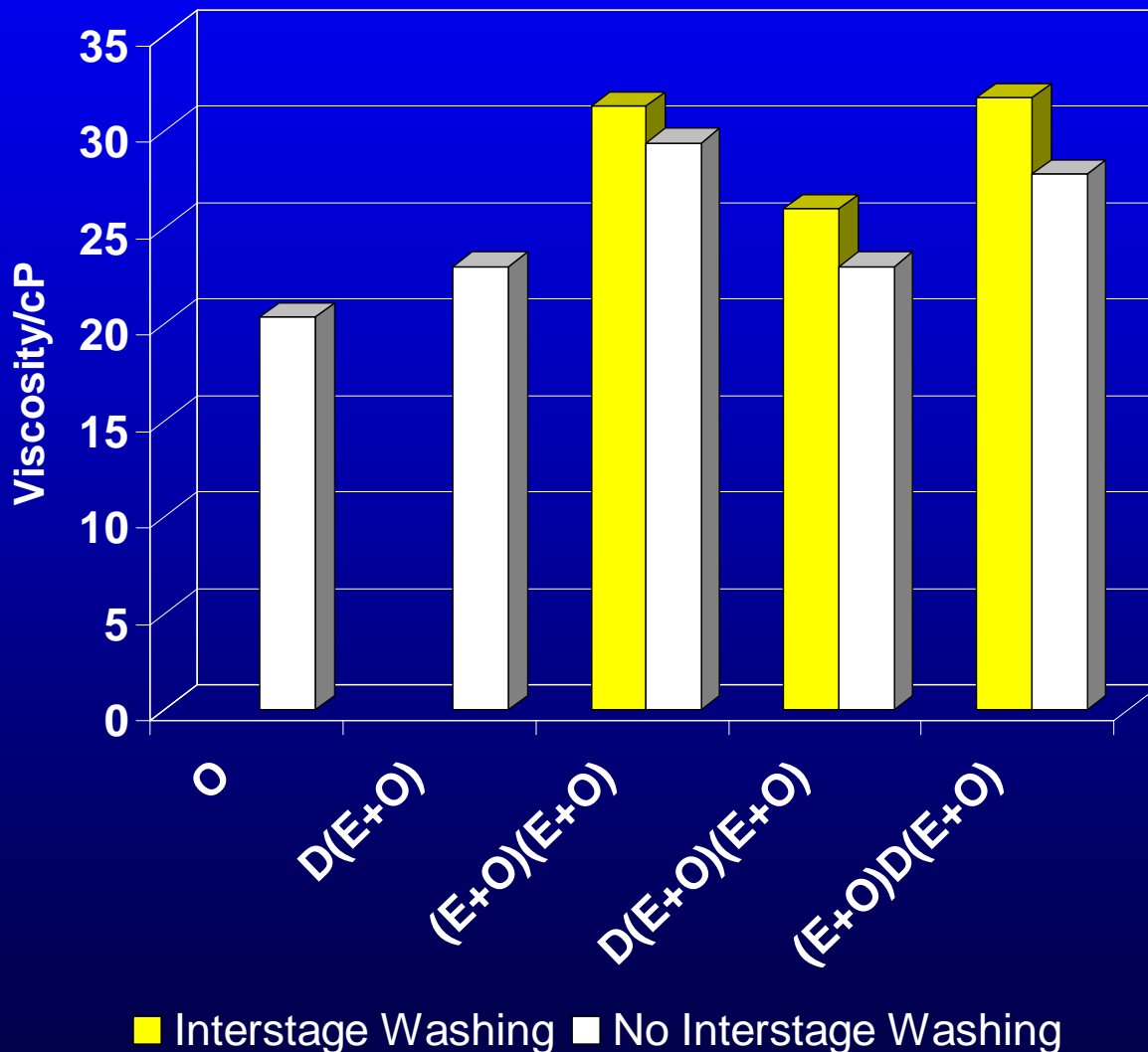
- (E+O) stage provides much more selectivity than a full O
- The D stage placement is important to the overall performance of the mini O

# Interstage Washing Effect on Kappa



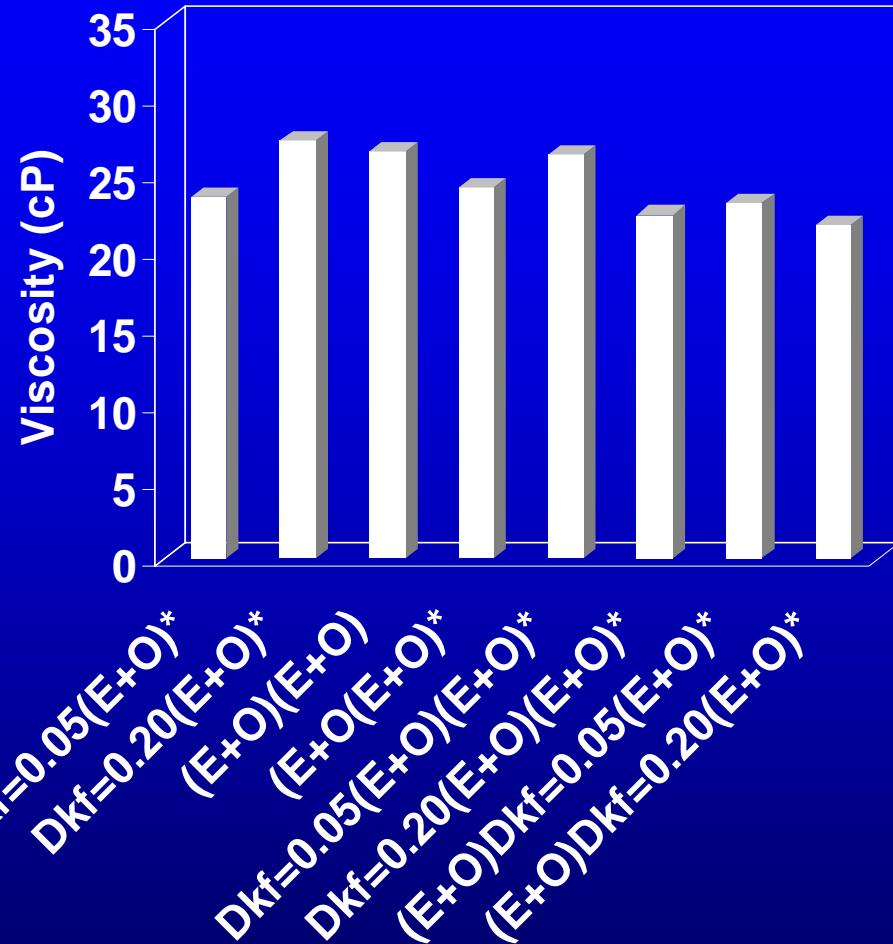
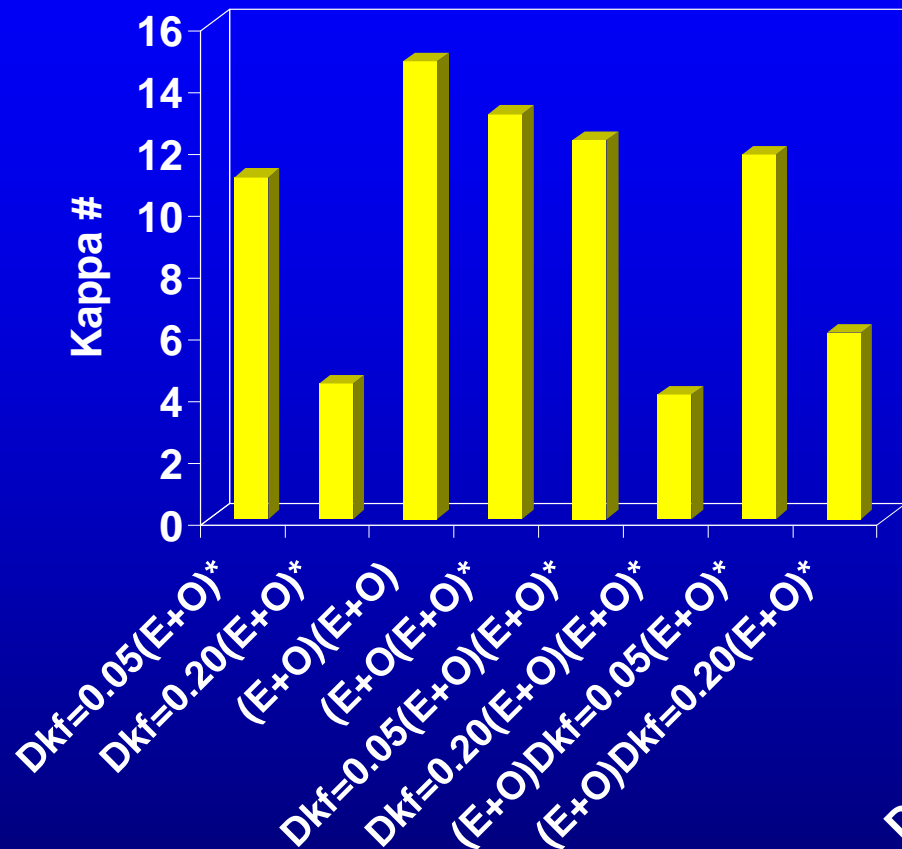
- Washing was done between the first and second stage
- Carryover appears to slightly enhance the delignification of the stage
- A slight increase in delignification obtained when D stage is after (E+O) in mini O

# Interstage Washing Effect on Viscosity



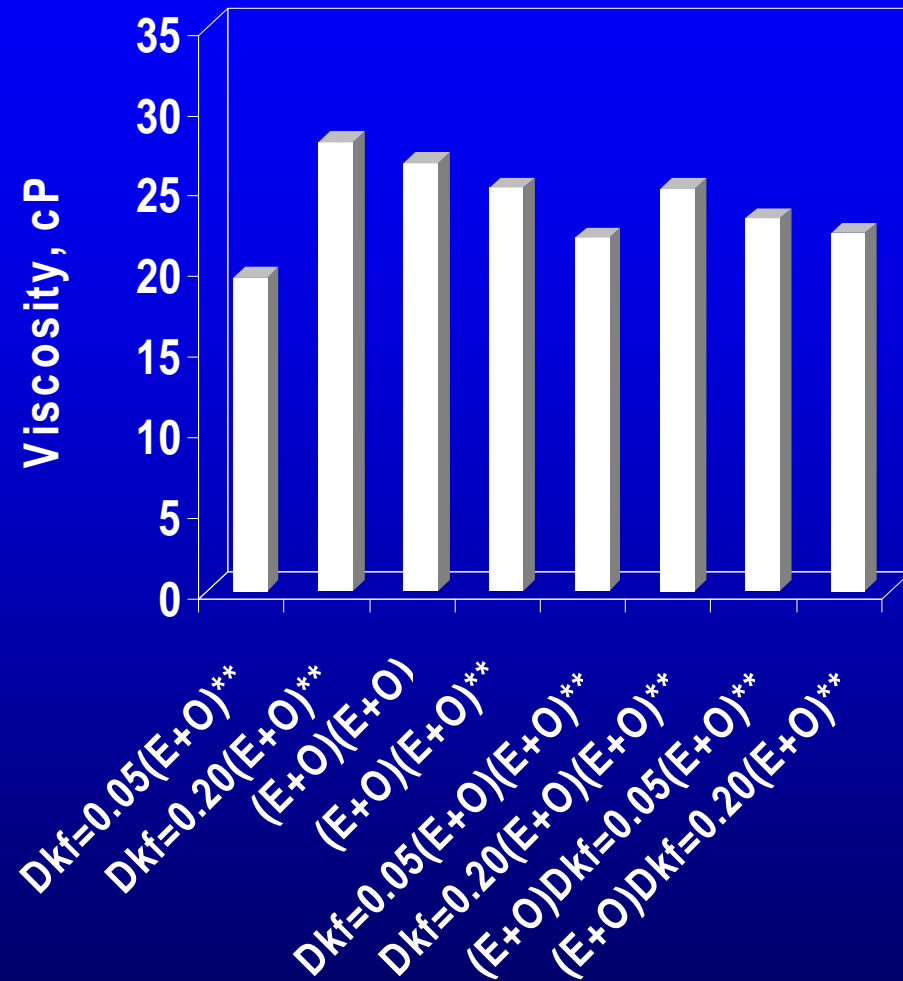
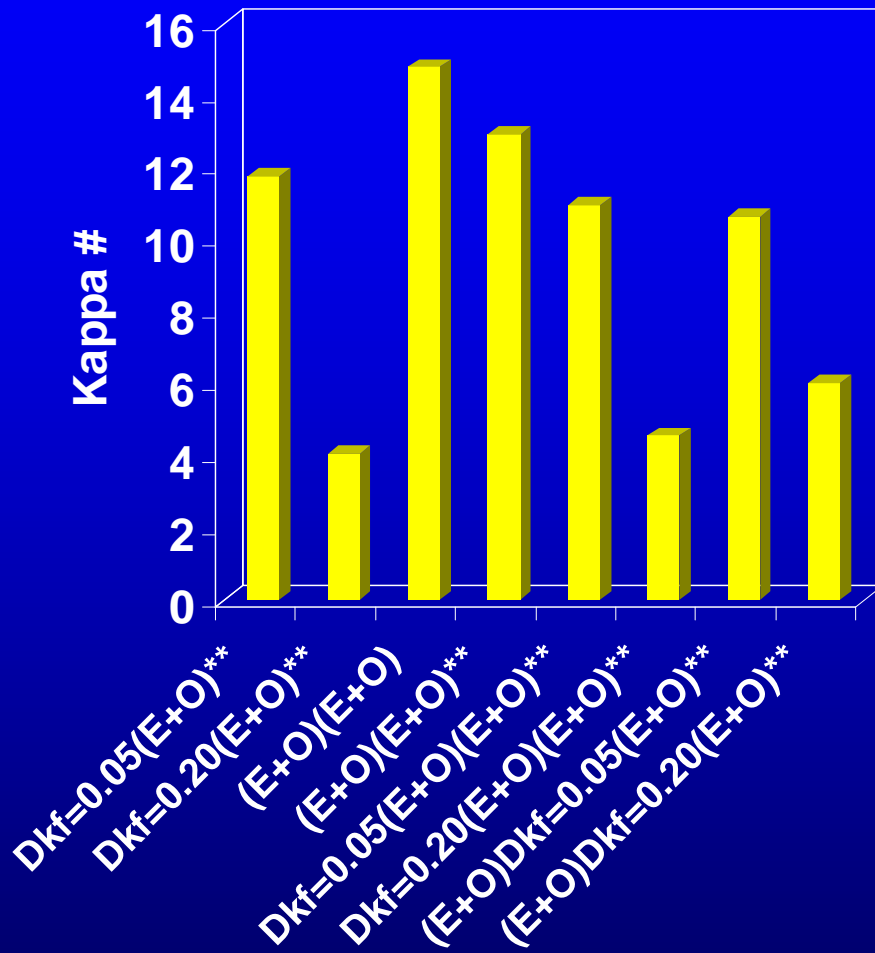
- In this case, washing slightly improves the viscosity of the pulp
- Loss in selectivity is therefore compensated by increase in delignification

# BL Carryover: 2kg/ton



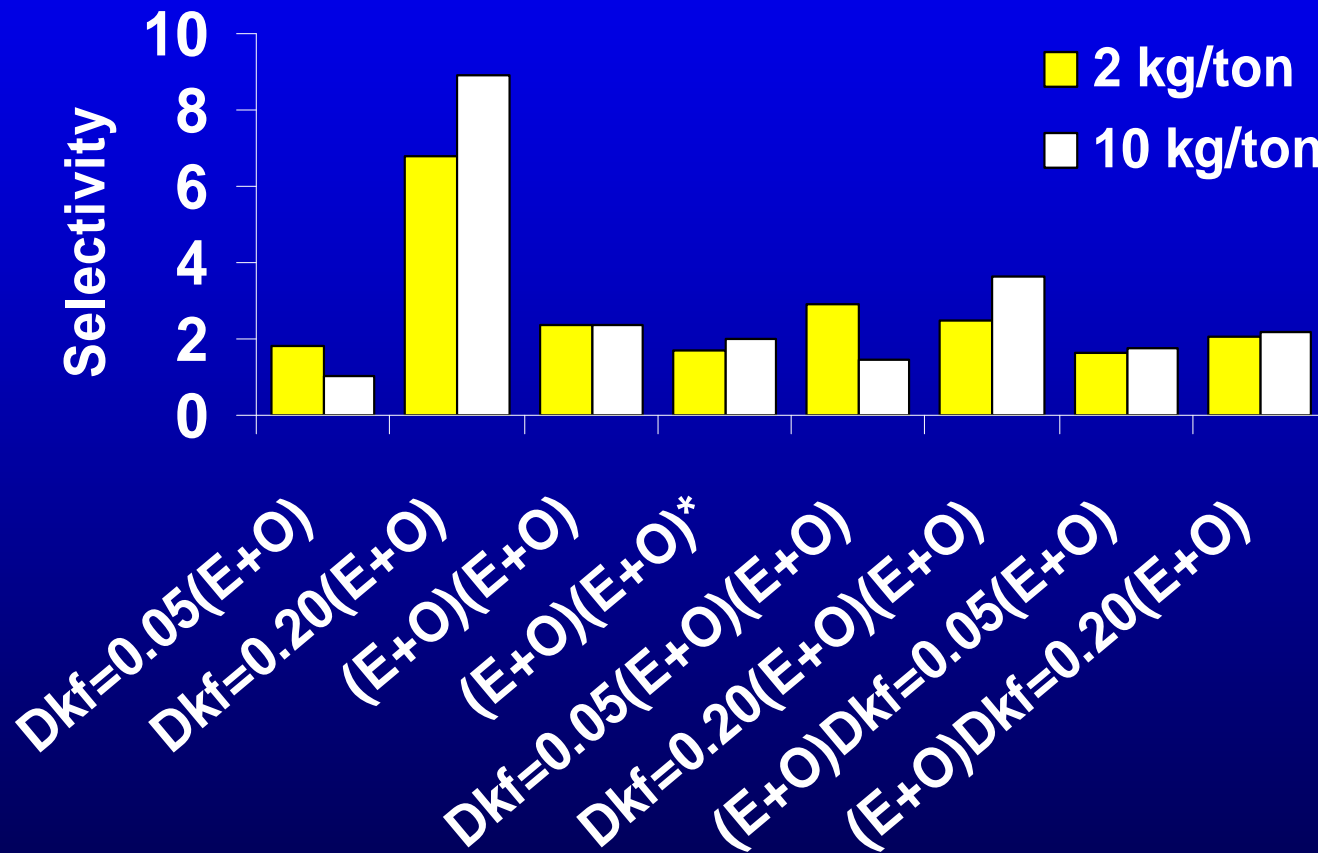
- The level of carryover does not have a pronounced effect on the levels of delignification obtained in the trials
- A slight drop in delignification does not have a major impact on viscosity

# BL Carryover : 10kg/ton



- In this case, the higher levels of carryover appear to reduce the delignification levels slightly
- Viscosity changes are not as pronounced as expected

# Summary of Selectivity Changes

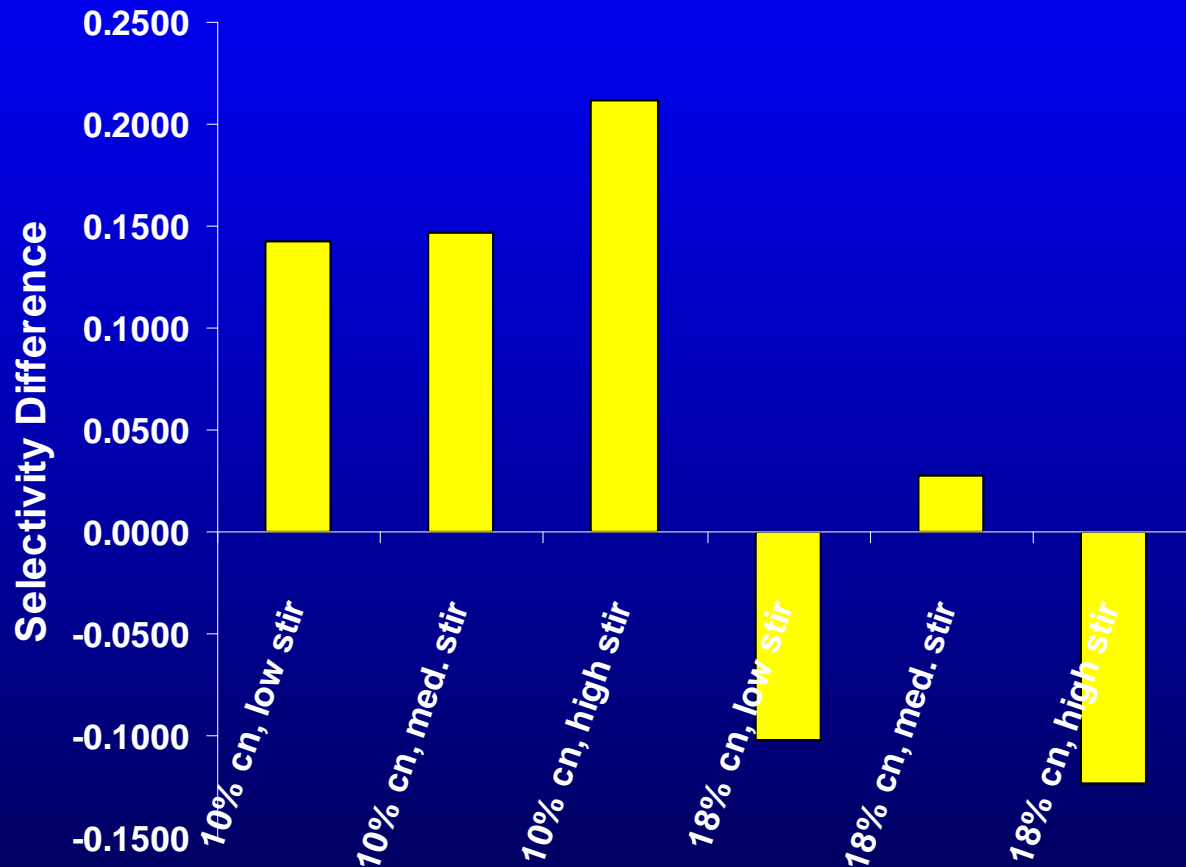


➤ **Increasing the number of (E+O) stages may have an impact on the overall selectivity**

# ***$^{31}\text{P}$ NMR Structural Elucidation***



# Oxygen Selectivity Trials

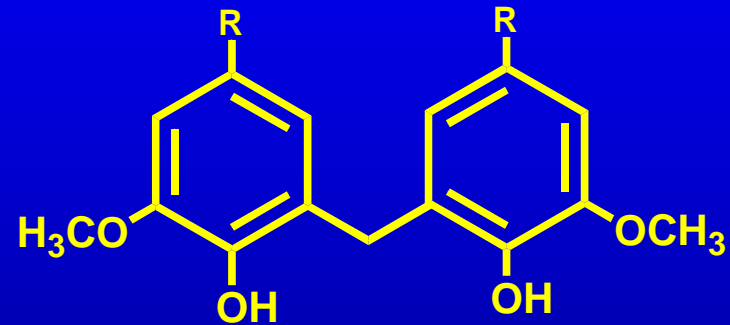
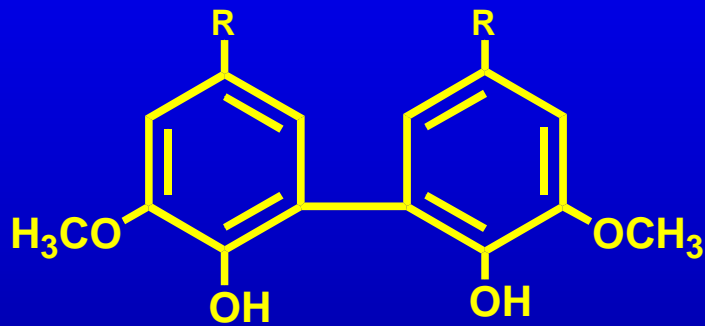


- All differences are based on a normalized selectivity (1) change
- Higher consistency pulps have lower selectivity trends as demonstrated from the literature
- Rates in stirring are based on a 5, 15, and 30 hz rate for 10 seconds every 5 minutes for one hour
- Basis of effect was investigated by NMR interrogation of effluents

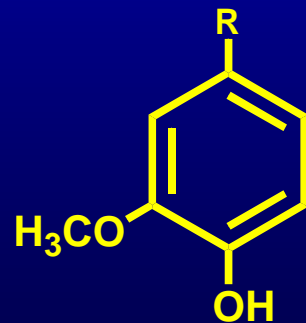
# Typical Phenolic Structures

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## 5,5'-Condensed Phenolic Subunits of Lignin

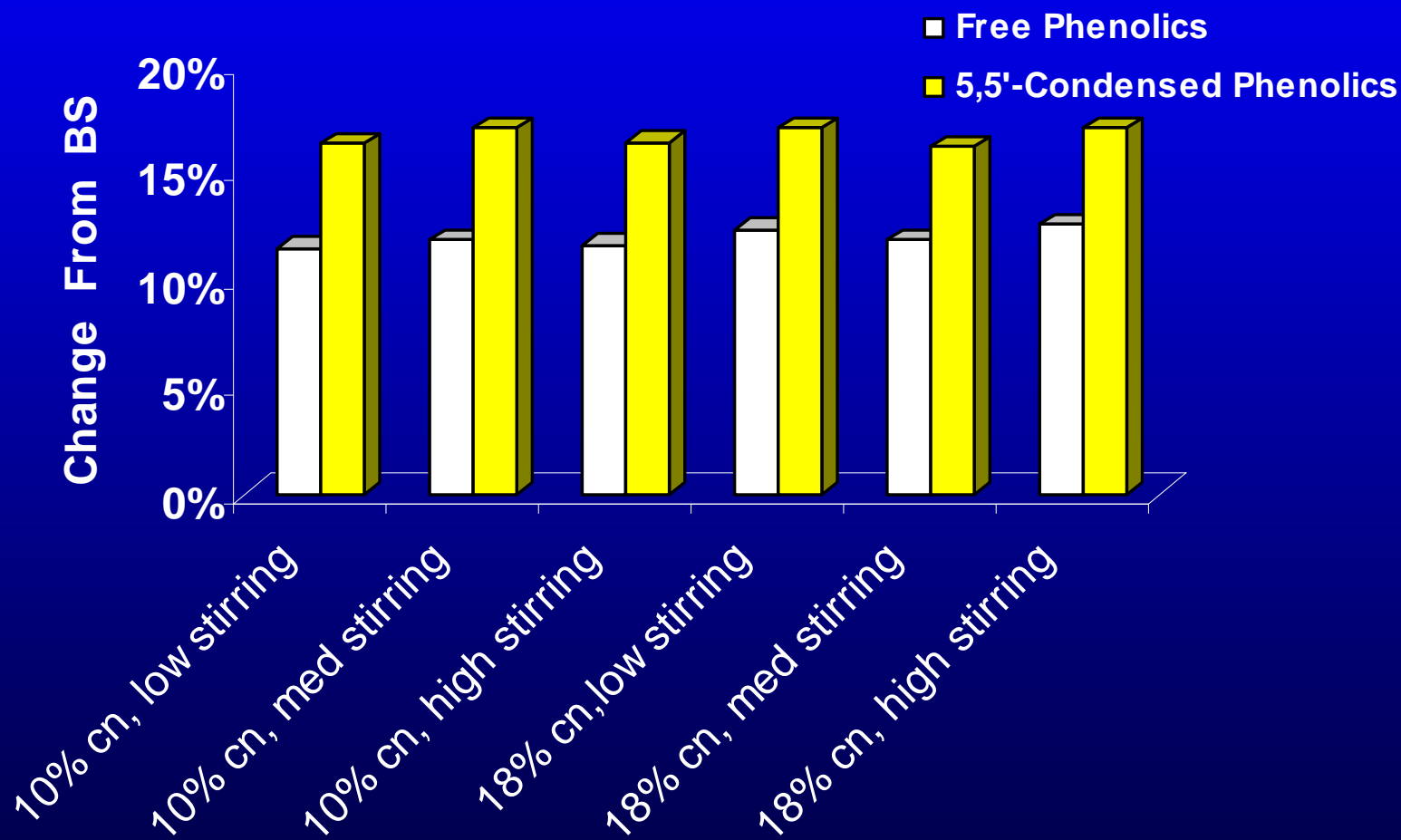


## Non-condensed (free) Phenolic Subunits of Lignin

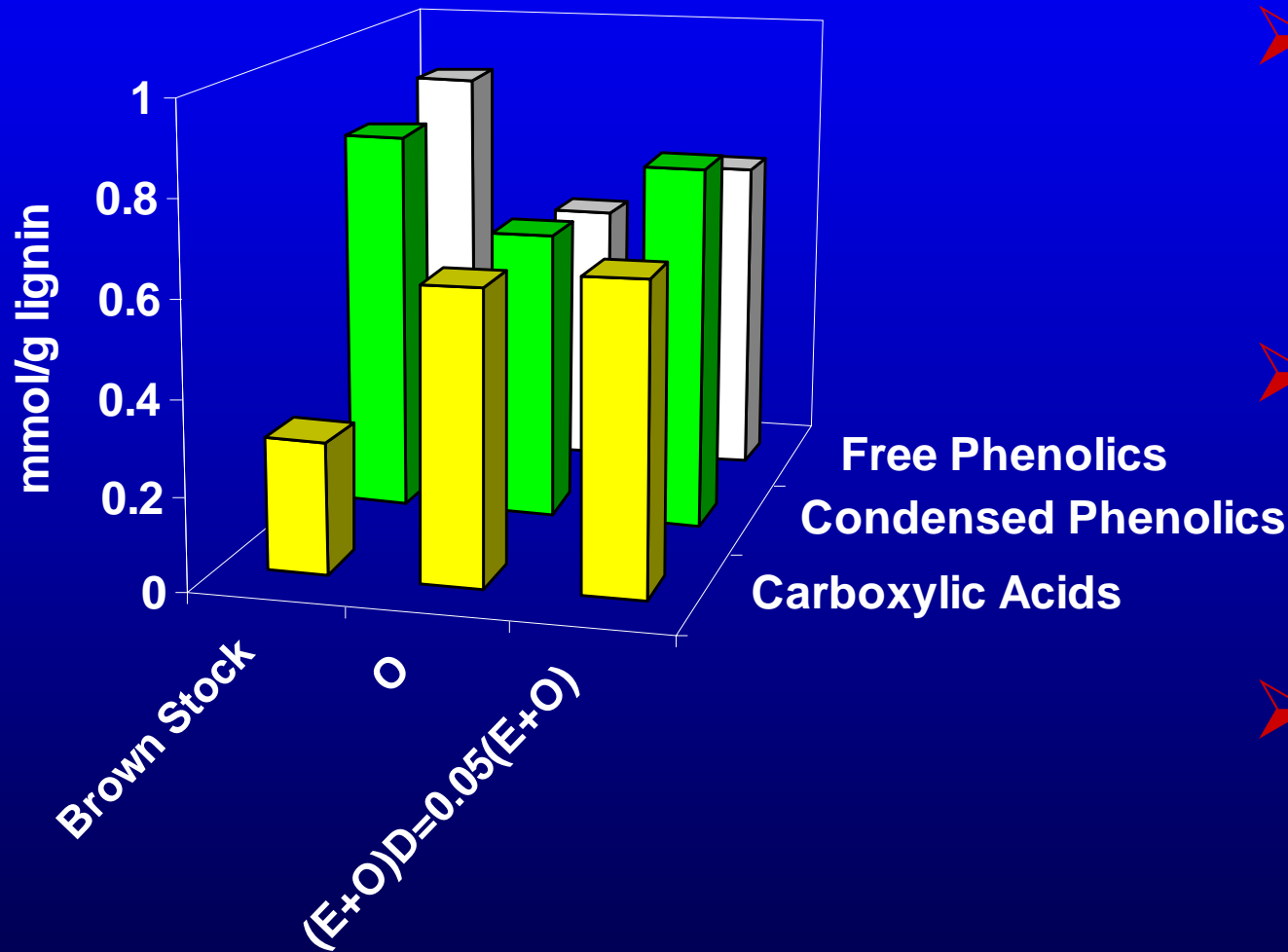


# Lignin Structural Differences Observed in O Effluent

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# Important Structural Differences

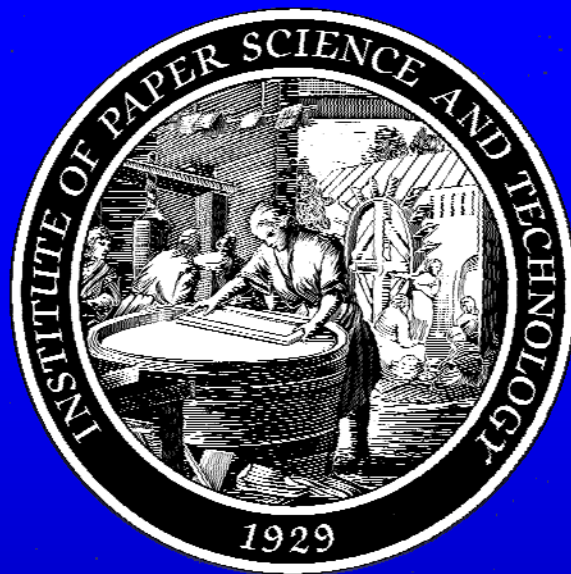


- $^{31}\text{P}$  NMR was used to evaluate the chemical differences
- Acid concentration did not change between the O and mini O
- Changes in phenolics are not as pronounced in mini O as in O

# Conclusions

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- **Mini O systems have some inherent pulp property benefits over full O**
- **Placement of D stage is important to the selectivity obtained**
- **The NMR studies from O and mini O systems suggest that the concentration of the condensed and non-condensed phenolics may not directly correlate with bleachability**



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